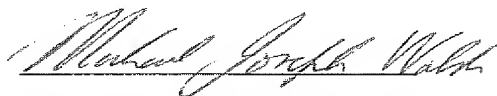


I, Michael Joseph Walsh, European Patent Attorney, of the firm of Tomkins & Co., Chartered Patent Agents and European Patent Attorneys, of 5 Dartmouth Road, Dublin 6, Ireland, hereby declare that I am conversant with the English and German languages and am a competent translator thereof. I declare further that to the best of my knowledge and belief the following is a true and correct translation of the accompanying documents in the German language, specifically a certified copy of German Patent Application No. 102 37 651.4 filed August 13 2002.



MICHAEL JOSEPH WALSH

The 14<sup>th</sup> day of August, 2009

**FEDERAL REPUBLIC OF GERMANY**

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**Priority Certificate  
for the Filing of a Patent Application**

File Number: 102 37 651.4  
Date of Filing: 13 August 2002  
Applicant / Owner: SCHÜMANN SASOL GmbH,  
Hamburg/Germany  
Title: Microcrystalline paraffin  
IPC: C 07 C 5/22

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Weihmayer

Patent Application

Microcrystalline Paraffin

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VGN 265 098 24581DE mue/har 13 August 2002

Microcrystalline paraffin

The invention relates to a microcrystalline paraffin, its preparation and its use.

5

Conventional microcrystalline paraffin obtained from mineral oil (also known as microwaxes) comprises a mixture of saturated hydrocarbons which are solid at room temperature and have a chain length distribution of  $C_{25}$  to  $C_{80}$ . In addition to n-alkanes, the microcrystalline paraffins contain highly branched isoalkanes and alkyl-substituted cycloalkanes (naphthenes) and proportions - even if generally small ones - of aromatics. The content of isoalkanes and of naphthenes is from 40 to 70%, determined according to EWF Standard Test Method for Analysis of Hydrocarbon Wax by Gas Chromatography. The quantitative dominance of the isoalkanes (and of the naphthenes) determines their microcrystalline structure.

20

The solidification range is between 50 and 100°C according to DIN ISO 2207. The needle penetration has values between  $2 \times 10^{-1}$  and  $160 \times 10^{-1}$  mm according to DIN 51579. The solidification point and the needle penetration are used for distinguishing among the microcrystalline paraffins between plastic and hard microcrystalline paraffins. Soft plastic microcrystalline paraffins (known as petrolates) are tacky with a very pronounced adhesive capability, and they have solidification points from 65 to 70°C and penetration values from 45 to  $160 \times 10^{-1}$  mm. The oil contents are from 1 to 15%. Plastic microcrystalline paraffins are readily deformable and kneadable and have solidification points between 65 and 80°C and penetration values from 10 to  $30 \times 10^{-1}$  mm. The oil contents may be up to 5%. The hard microcrystalline paraffins are tough and slightly tacky with

35

solidification points from 80 to 95°C and penetration values from 2 to 15 x 10<sup>-1</sup> mm. The oil contents are not more than 2% (cf. Ullmanns Enzyklopädia of Industrial Chemistry, VCH-Verlagsgesellschaft 1996).

5

Microcrystalline paraffins have a high molar mass and hence high boiling points. They have been obtained to date from the residues of vacuum distillation of mineral oil, in particular in the production of lubricating oil (residue waxes), and from deposits of the mineral oil during its recovery, its transport and its storage, specifically in technologically very complicated and expensive processes having a plurality of stages, for example deasphalting, solvent extraction, dewaxing, deoiling and refining. The deoiled microcrystalline paraffins contain, as impurity, sulfur, nitrogen and oxygen compounds. They are accordingly not entirely odorless and have a dark yellow to dark brown color. The refinement therefore required is effected, depending on the later application, by bleaching (industrial applications) or by hydrotreating (applications in the food industry and pharmaceutical industry).

Microcrystalline paraffins are used predominantly as mixing components in paraffin or wax mixtures. However, they are mostly used in ranges up to 5%. In particular, hardness and melting point of these mixtures are to be increased and flexibility and oil binding capacity improved. Typical applications are, for example, the preparation of waxes for impregnation, coating and lamination for the packaging industry and textile industry, of heatseal and hotmelt adhesives and of pharmaceutical and cosmetic products, including chewing gum. Furthermore, they are used in casting compounds and cable materials and generally in plastics, but also

in the candle, rubber and tire industries and in care, antislip and anticorrosion compositions.

DE 69 418 388 T2 describes a hydroisomerization of  
5 n-paraffins that are solid at room temperature and have  
more than 15 C atoms by use of a catalyst based on a  
metal of group VIII, in particular platinum, and a  
borosilicate having a  $\beta$ -zeolite structure to give  
products which are suitable for the preparation of  
10 lubricating oils. (Page 1)

DE 695 15 959 T2 describes the hydroisomerization of  
wax-containing starting materials to give products  
which are suitable for the preparation of lubricating  
15 oils. A temperature from 270° to 360°C and a pressure  
from 500 to 1,500 psi or from 3.44 MPa to 10.36 MPa is  
used for this. The catalyst is based on a catalyzing  
metal component on a porous, heat-resistant metal oxide  
carrier. (cf. page 2, paragraph 1), in particular on  
20 from 0.1 to 5% by weight of platinum on alumina or  
zeolites, such as, for example, offretite, zeolite X,  
zeolite Y, ZSM-5, ZSM-2, etc. (cf. page 3, middle). The  
starting materials to be isomerized may be any wax or  
wax-containing material, in particular also a Fischer-  
25 Tropsh wax (cf. page 5, middle). The hydrogen is fed  
to the reactor at a rate of 1,000 to 10,000 SCF/bbl and  
the wax at from 0.1 to 10 LHSV (cf. page 6, middle).  
The isomerization product is liquid (cf. page 7, line  
7). It can be fractionated by distillation or by  
30 treatment with solvents, for example with an  
MEK/toluene mixture (cf. page 7, last paragraph).

The entire liquid product from the isomerization plant  
is more advantageously treated in a second stage under  
35 mild conditions with use of the isomerization catalyst  
based on a noble metal of group VIII and a heat-  
resistant metal oxide, in order to reduce PNA and other

impurities in the isomerization product and thus to obtain an oil having improved daylight stability (cf. page 8, paragraph 2). Mild conditions are to be understood as meaning: a temperature in the range from about 170° to 270°C, a pressure from about 300 to 1500 psi, a hydrogen gas rate from about 500 to 1 000 SCF/bbl and a flow rate from about 0.25 to 10 vol./vol./h.

The production data for the reactor is 0.2 to 2 v/vh. The hydrogen is fed to the reactor at a rate from about 0.089 to 2.67 m<sup>3</sup> H<sub>2</sub> per 1 l of wax. The catalyst has a decisive influence on the conversion. If it is based on platinum and a β-zeolite having a pore diameter of about 0.7 nm, the desired conversion to a middle distillate product is not observed, in particular with decreasing temperature to 293.9°C (cf. example 3).

In comparison, it is an object of the invention to provide a novel microcrystalline paraffin, a process for its preparation and a use for this microcrystalline paraffin.

This object is first and foremost achieved by the subject matter of claim 1 (product) or of claim 5 (process) or of claim 10 (use). The aim here is to obtain the microcrystalline paraffin, preparable by catalytic hydroisomerization at temperatures above 200°C, from paraffins containing Fischer-Tropsch synthesis (FT paraffins) with a C chain length distribution in the range from C<sub>20</sub> to C<sub>105</sub>. Surprisingly, it has been found that such a microcrystalline paraffin is free of naphthenes and aromatics. It is furthermore surprising that, in spite of isomerization, crystallinity has been retained. Continuous preparation with defined properties is facilitated. Production is also possible in a stepwise process. A product in the

low and high solidification point range, to be referred to as a microwax, is provided. A continuous or batchwise catalytic hydroisomerization of Fischer-Tropsch paraffins (FT paraffins) can be carried out.

5 Regarding FT paraffins as such, reference should be made in particular to the statements by A. Kühnle in Fette, Seifen, Anstrichmittel [Fats, soaps, coating compositions], 84th year, page 156 et seq., "Fischer-Tropsch-Wachse Synthese, Struktur, Eigenschaften und

10 Anwendungen [Fischer-Tropsch waxes, synthesis, structure, properties and applications]". In summary, the FT paraffins are paraffins which were prepared according to the Fischer-Tropsch process by known routes from synthesis gas (CO and H<sub>2</sub>) in the presence

15 of a catalyst at elevated temperature. They are the highest boiling fraction of the hydrocarbon mixture. Substantially long-chain, slightly branched alkanes, which are free of naphthenes and aromatics and of oxygen and sulfur compounds, are formed thereby.

20 Such FT paraffins having a high proportion of n-paraffins and a C chain length in the range from C<sub>20</sub> to C<sub>105</sub> are converted by the process described here into microcrystalline paraffins having a high melting point

25 and a high proportion of isoparaffins.

According to the process aspect of the invention, the microcrystalline paraffin can be prepared by catalytic isomerization as follows:

- 30
- A. use of FT paraffin as starting material
- a) having a C chain length in the range from C<sub>20</sub> to C<sub>105</sub>,
  - b) preferably having a solidification point in the
  - 35 range from 70 to 105°C, in particular about 70, 80, 95 or 105°C according to DIN ISO 2207,
  - c) a penetration at 25°C from 1 to 15;

d) a ratio of isoalkanes to n-alkanes from 1 : 5  
to 1 : 11

5 B. use of a catalyst, preferably in the form of  
extrudates, spheres, pellets, granules or powders,  
suitably based on

a) 0.1 to 2.0, in particular 0.4 to 1.0, % by  
mass, based on the catalyst calcined at 800°C,  
of hydrogenating metal of the eighth subgroup,  
10 in particular platinum, and

b) a support material comprising a zeolite having  
a pore diameter in the range from 0.5 to 0.8 nm  
(from 5.0 to 8.0 Å),

15 C. use of a process temperature of more than 200°C,  
in particular from 230 to 270°C,

D. use of a pressure from 2.0 to 20.0, in particular  
from about 3 to 8, MPa in the presence of hydrogen  
20 and a ratio of hydrogen to FT paraffin from 100 :  
1 to 1 000 : 1, in particular from about 250 : 1  
to 600 : 1, Nm<sup>3</sup>/m<sup>3</sup>.

Suitably, the loading of the reactor with the FT  
25 paraffin is in the range from 0.1 to 2.0, in particular  
0.2 to 0.8, v/v.h (volume of FT paraffin per volume of  
the reactor within one hour).

The yield of hydroisomerization products is between 90  
30 and 96% by mass, based on the FT paraffin used in each  
case. With regard to alkanes having a low melting  
point, the hydroisomerization products obtained also  
contained alkanes in the C chain length range  $\leq C_{20}$  up  
to 5% (usually up to 3%). These alkanes could be  
35 readily separated off by vacuum distillation with  
steam.

The catalyst used is preferably based on a  $\beta$ -zeolite. The catalyst may be formed on a base of powder or of particles. Noble metals may be changed into the  $\beta$ -zeolite, for example by a cationic bond in accordance with known methods. The  $\beta$ -zeolite has an  $\text{SiO}_2$  to  $\text{AlO}_3$  mole ratio of 20 : 1 to 100: 1 (e.g. 25, 30, 35, 40, 45, 50, 55, 60, 65, 70, 75, 80, 85, 90, 95 : 1) and contains less than 0.02% of alkali oxide based on the dry matter.

The catalytic hydroisomerization of the FT paraffins is preferably carried out continuously in a flow-through reactor using a fixed-bed catalyst, in particular in the form of extrudates, spheres or pellets, it being possible for the flow through the reactor to be either from top to bottom or from bottom to top when said reactor is oriented vertically, as is preferred. However, the process can also be carried out batchwise in a batch process in, for example, a stirred autoclave, the catalyst being contained in a permeable net or being used finely distributed as granules or powder in the FT paraffin. The process parameters of the continuous and of the batchwise process are the same.

The microcrystalline paraffins obtained according to the invention have the following properties:

Compared with the FT paraffins used, they have lower solidification points and contain, in addition to n-alkanes, a high, in particular higher, proportion by weight of isoalkanes than of n-alkanes. The proportion of n-alkanes or isoalkanes is determined by gas chromatography. The increased degree of isomerization achieved by the hydroisomerization is expressed in increased penetration values, a reduced crystallinity and a reduced enthalpy of fusion. Moreover, these

products have a pasty to tacky viscous consistency with a somewhat crumbly appearance.

5 The crystallinity is determined by X-ray diffraction analysis. It defines the crystalline fraction of the product obtained in relation to the amorphous fraction. The amorphous fractions lead to different diffraction of the X-rays than is the case for the crystalline fractions. The needle penetration at 25°C in the case  
10 of the products according to the invention is in the range from 20 to 160, measured according to DIN 51579. The products obtained are solid at 20°C, in the sense that they do not run.

15 The crystalline fraction is reduced in particular as follows: while the starting material has a crystalline fraction in a range from 60 to 75%, a crystalline fraction of 30 to 45% is observable in the case of the hydroisomerization product, in particular in the range  
20 from 35 to 40 (36, 37, 38, 39) %.

The crystalline fractions and the amorphous fractions are given by said X-ray diffraction analysis in each case in % by mass.

25 The microcrystalline paraffins prepared according to the invention from FT paraffins have physical and material properties which are similar or comparable to those of microcrystalline paraffins based on mineral  
30 oil (microwaxes).

The microcrystalline paraffins prepared by catalytic hydroisomerization can also be deoiled using a solvent. However, this does not mean that the hydroisomerization  
35 products described have a content of conventional oil. In any case, however, very short-chain n-alkanes or isoalkanes are removed. By use of a solvent mixture of

95 : 5 parts by volume of dichloroethane : toluene and  
a product/solvent ratio of 1 : 3.6 parts at 22°C, a  
deoiled microcrystalline paraffin is obtained in a  
yield from 80 to 90% by weight, based on the  
5 hydroisomerization product used. It has the following  
properties

:

- Needle penetration: from  $1 \times 10^{-1}$  to  $7 \times 10^{-1}$ , in  
particular from  $3 \times 10^{-1}$  to  $6 \times 10^{-1}$ , mm, determined  
10 according to DIN 51579,
- oil content: from 1.0 to 2% by weight, in  
particular from 1.2 to 1.6% by weight, determined  
by MIBK according to modified ASTM D 721/87
- solidification point: from about 60 to about 95°C,  
15 in particular 70 to 85°C, determined according to  
DIN ISO 2207.

Removing the oil thus converted the medium-hard product  
into a hard product when it is compared with the types  
20 based on mineral oil. The deoiled hydroisomerization  
product is then comparable with the hardest types based  
on mineral oil.

Owing to its properties, the microcrystalline  
25 hydroisomerization product prepared according to the  
invention and the corresponding deoiled  
microcrystalline hydroisomerization product can be used  
as a microwax (cf. introduction). In particular, the  
hydroisomerization product obtained can also be  
30 oxidized. Oxidized products are obtained which differ  
according to melting range and degree of oxidation and  
are used in particular as corrosion inhibitors and as  
cavity and underfloor protection compositions for motor  
vehicles. They are moreover used in emulsions as care  
35 compositions and release agents and as additives for  
printing ink materials and carbon paper coloring  
materials.

The acid and ester groups, which are randomly distributed over hydrocarbon chains, can be reacted with inorganic or organic bases to give water-dispersible formulations (emulsifiable waxes) and lead to products having very good metal adhesion.

Further fields of use are the preparation of impregnating, coating and laminating waxes for the packaging and textile industries, heatseal and hotmelt adhesives, as a blend component in candles and other wax products, in wax mixtures for crayons, floor care compositions and automotive care compositions and for dental technology and pyrochemistry.

They are furthermore a component of light stabilizer waxes for the tire industry, electrical insulation materials, framework and pattern waxes for the precision casting industry and wax formulations for explosives, munitions and propellant technology.

Such products are furthermore suitable as release agents in the pressing of wood, chip and fiber boards, in the production of ceramic parts and, owing to their retentivity, for the production of solvent-containing care compositions, grinding pastes and polishing pastes and as dulling agents for finishes.

Furthermore, these products can be used for the formulation of adhesive waxes, cheese waxes, cosmetic preparations, chewing gum bases, casting materials and cable materials, sprayable pesticides, vaselines, artificial firewood, lubricants and hotmelt adhesives.

A test for food safety is carried out, for example, according to FDA, § 175.250.

The invention will now be explained in detail with reference to examples.

Example 1:

5

An FT paraffin having a solidification point at 97°C was catalytically isomerized with hydrogen at a pressure of 5 MPa (50 bar), a temperature of 270°C and a v/vh ratio of 0.3. The resulting hydroisomerization was demonstrated by characteristics in table 1.

10

Before hydroisomerization was initiated, the catalyst comprised 0.8% by mass of platinum on  $\beta$ -zeolite and an  $\text{SiO}_2$  to  $\text{Al}_2\text{O}_3$  molar ratio of 23:1. The catalyst was present in hydrogen form. It contained less than 0.02% of alkali oxide on a dry basis.

15

The hydroisomerization product is white, odorless and slightly tacky and thus differs substantially from the brittle starting material. The isoalkane fraction is increased about 6-fold, which is demonstrated by the increased penetration value, the reduced crystallinity and the reduced enthalpy of fusion. On the basis of its characteristics, the synthetic, microcrystalline paraffin thus prepared is to be classified between a plastic and a hard microwax based on mineral oil. The hydroisomerization product was thus a paraffin having a pronounced microcrystalline structure, whose C chain length distribution of 23 to 91 carbon atoms corresponds approximately to that of the starting material with 27 to 95, but shifted toward smaller chain lengths. The chain length was determined by gas chromatography.

20

25

30

35 Example 2:

An FT paraffin having a solidification point at 70°C was catalytically isomerized with hydrogen at a pressure of 5 MPa (50 bar), a temperature of 250°C and a v/vh ratio of 0.3. The resulting structural conversion was demonstrated by the characteristics in the table.

The same catalyst was used as in Example 1.

The hydroisomerization product is white and odorless as well as pasty and slightly tacky. The isoalkane fraction is increased about 5-fold. The high degree of isomerization is expressed in the substantially increased penetration value, the reduced crystallinity and the reduced enthalpy of fusion. The microcrystalline paraffin thus obtained has a similar but slightly reduced C chain length compared with the FT paraffin, which is clear from the carbon atoms: 23 to 42 in the case of the hydroisomerization product and 25 to 48 in the case of the FT paraffin. On the basis of its characteristics, the synthetic microcrystalline paraffin thus prepared is comparable to a soft plastic microcrystalline paraffin obtained on the basis of mineral oil.

Examples 1 and 2 show that, by means of the process according to the invention, the FT paraffins, which predominantly comprise n-alkanes and have a fine crystalline structure and a brittle consistency, were converted into nonfluid, pasty or solid paraffins which have lower melting points than the starting materials. These paraffins are distinguished by a high content of branched alkanes and consequently have a microcrystalline structure with substantially reduced crystallinity and a plastic to slightly tacky consistency. The branched alkanes are predominantly methyl-alkanes, the methyl groups preferably occurring

in the 2-, 3-, 4- or 5-position. Multiply methyl-branched alkanes were also formed to a small extent.

The results of examples 1 and 2, also compared with the starting material, are listed in the attached table 1.

Example 3:

A catalyst (cylindrical extrudate, diameter 1.5 mm, length about 5 mm) was used in uncommunuted form. 92 ml of catalyst were introduced in undiluted form into the reactor tube (total volume 172 ml, internal diameter 22 mm). The catalyst zone was also covered with a layer of the earth material. A thermocouple was positioned in the reactor in such a way that the temperature was measured at a depth of 2 cm and 17 cm in the catalyst bed. The catalysts were dried and activated (by means of high temperature, water is expelled and platinum reduced).

The paraffin starting material used was an FT paraffin C80 (solidification point 81°C, n-paraffin/isoparaffin mass ratio: 93.9/6.1). The oil content of the starting material was 0.5%. The needle penetration value was 6.0.

The experiments were carried out at a hydrogen pressure of 50 bar.

The following results were obtained: at 260°C and 0.96 v/v.h, the iso fraction (% by mass) increased from 6.1 (FT paraffin) to 42 (hydroisomerization product). The solidification point was 77°C and the oil content 18.8%. The needle penetration value was 32.

The catalyst was a platinum catalyst on  $\beta$ -zeolite. Regarding  $\beta$ -zeolites, reference is made to the

publication "Atlas of Zeolite Structure Types",  
Elsevier Fourth Revised Edition, 1996.

Gas chromatograms obtained for this example are  
5 attached as an appendix.

In contrast to the microcrystalline paraffins obtained  
from mineral oil, the completely synthetic  
microcrystalline paraffins prepared by the  
10 hydroisomerization according to the invention contain  
no highly branched isoalkanes, no cyclic hydrocarbons  
(naphthenes) and in particular no aromatics and sulfur  
compounds. They thus meet the highest purity  
requirements for microcrystalline paraffins and are  
15 therefore outstandingly suitable for use in the  
cosmetic and pharmaceutical industries and for  
packaging and preservation in the food industry.

Table: Characteristics of starting materials and reaction products

Characteristics	Unit	Method of measurement	Example 1		Example 2	
			FT paraffin	Hydroisomer-ization	FT paraffin	Hydroisomer-ization
Solidification point	°C	DIN ISO 2207	97.0	86.5	71.5	61.5
Penetration N at 25°C	0.1 mm	DIN 51579	2	42	13	98
Enthalpy of fusion	J/g	ASTM D4419	221	127	195	120
Crystallinity	% by mass	X-ray diffraction analysis	70.7	43.5	62.4	38.8
n-/iso-alkane weight ratio	%	Gas chromatography	88/12	37/63	91/9	43/57
Oil content (MIBK)	% by mass	ASTM D721-87 (modified)	0.66	14.6	0.4	23.1

# CLAIMS

1. Microcrystalline paraffin, preparable by catalytic hydroisomerization at temperatures above 200°C  
5 from FT paraffins having a C chain length distribution in the range from 20 to 105.
2. Microcrystalline paraffin according to claim 1 or in particular according thereto, characterized in  
10 that it is nonfluid at 25°C but at least pasty with a needle penetration of less than  $100 \times 10^{-1}$ , measured according to DIN 51579.
3. Microcrystalline paraffin according to claim 1 or in particular according thereto, characterized in  
15 that it is free of aromatic heterocyclic compounds.
4. Microcrystalline paraffin according to claims 1, 2 or 3 or in particular according thereto,  
20 characterized in that the proportion by weight of the isoalkanes is greater than that of the n-alkanes.
- 25 5. Process for the preparation of a microcrystalline paraffin, in particular of a microcrystalline paraffin according to one of claims 1 to 4, by catalytic hydroisomerization by  
30 A. use of FT paraffins as starting material having carbon atoms in the range from 20 to 105 and  
B. use of a catalyst  
35 C. use of a process temperature of more than 200°C and

D. action of pressure in the presence of hydrogen.

6. Process according to claim 5 or in particular according thereto, characterized by the use of a catalyst based on a zeolite, preferably  $\beta$ -zeolite having a pore size between 0.50 and 0.80 nm, as support material, and a metal of the 8th subgroup as active component.
7. Process according to one of claims 5 or 6 or in particular according thereto, characterized in that it proceeds at raised pressure and elevated temperature.
8. Process according to one of claims 5 or 7 or in particular according thereto, characterized by a process temperature of 200 to 300°C.
9. Process according to one of claims 5 to 8 or in particular according thereto, characterized in that the pressure is 2 to 20 MPa.
10. Process according to one of claims 5 to 9 or in particular according thereto, characterized in that the pressure is 3 to 8 MPa.
11. Process according to one of claims 5 to 10 or in particular according thereto, characterized by a process temperature of 230 to 270°C.
12. Process according to one of claims 5 to 8 or in particular according thereto, characterized by a feed ratio of hydrogen to FT paraffin of 100 : 1 to 1 000 : 1 Nm<sup>3</sup> per m<sup>3</sup>.
13. Process according to one of claims 5 to 12 or in particular according thereto, characterized by a

feed ratio of hydrogen to FT paraffin of 250 : 1 to 600 : 1 Nm<sup>3</sup> per m<sup>3</sup>.

- 5           14. Process according to one of claims 5 to 13 or in particular according thereto, characterized in that a loading of 0.1 to 2.0 v/vh, preferably 0.2 to 0.8 v/vh, is employed.
- 10           15. Process according to one of claims 5 to 14 or in particular according thereto, characterized in that the catalyst has a pore size between 0.55 and 0.76 nm.
- 15           16. Process according to one of claims 5 to 15 or in particular according thereto, characterized in that the catalyst has a hydrogenation metal component of subgroup VIII of the Periodic Table of the Elements.
- 20           17. Process according to one of claims 5 to 16 or in particular according thereto, characterized in that the catalyst has platinum as hydrogenation metal.
- 25           18. Process according to one of claims 5 to 17 or in particular according thereto, characterized in that the platinum content of the catalyst is 0.1 to 2.0% by mass, preferably 0.4 to 1.0% by mass, based on the catalyst calcined at 800°C.
- 30           19. Process according to one of claims 5 to 18 or in particular according thereto, characterized in that the FT paraffin is used in a solidification point range of 70 to 105°C, preferably with solidification points of 70, 80, 95 or 105°C.
- 35

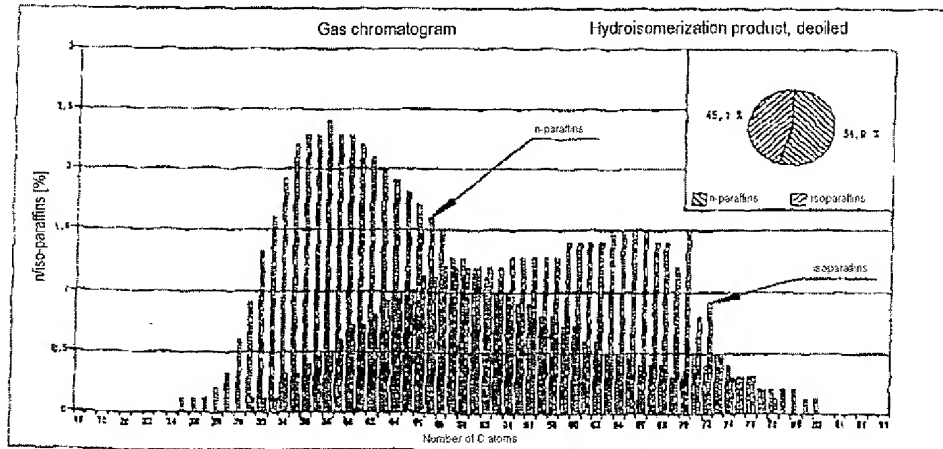
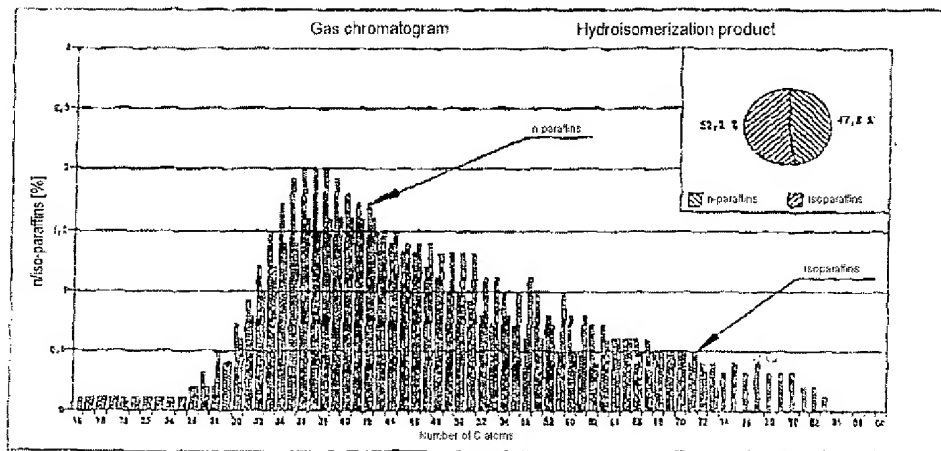
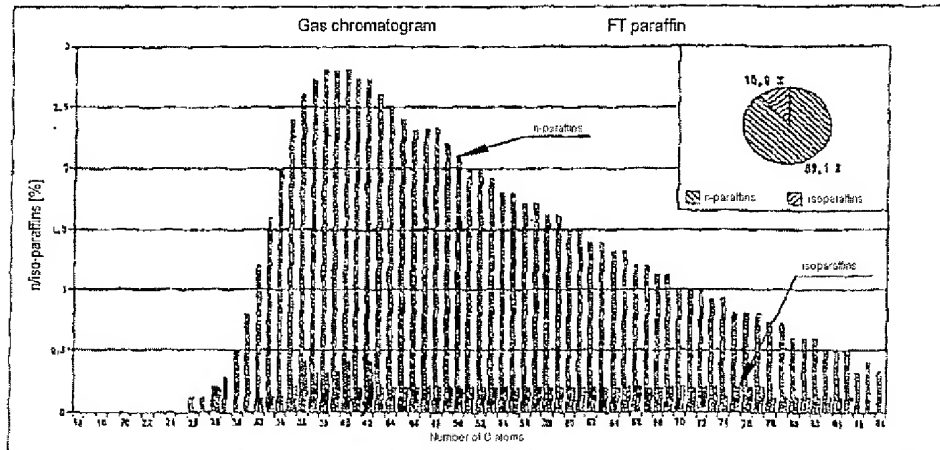
20. Use of the microcrystalline paraffins according to claims 1 to 4 and the microcrystalline paraffins prepared according to process claims 5 to 9 in the pharmaceutical or cosmetic sector or in the food industry.
- 5

Abstract

Microcrystalline paraffin

5 A novel, completely synthetic microcrystalline paraffin  
is described, which can be obtained in a simple manner  
and with a high yield by catalytic hydroisomerization  
of FT paraffins with 20 to 105 carbon atoms. They are  
pasty to solid at room temperature and have a higher  
10 percentage of iso-paraffins than n-paraffins. They  
contain no aromatics. Thus they are suitable in  
particular for pharmaceutical and cosmetic uses as well  
as in the foodstuffs industry.

### Gas chromatograms for Example 3



tran 2095 (ex-0575): MP3562 (ex-2151): Rieder 24 581 N2 PCT (ex-24077 N1  
PCT): 1<sup>st</sup> pr doc, Aug 11, 2009 (ex-literal, Jan 10, 2003)